

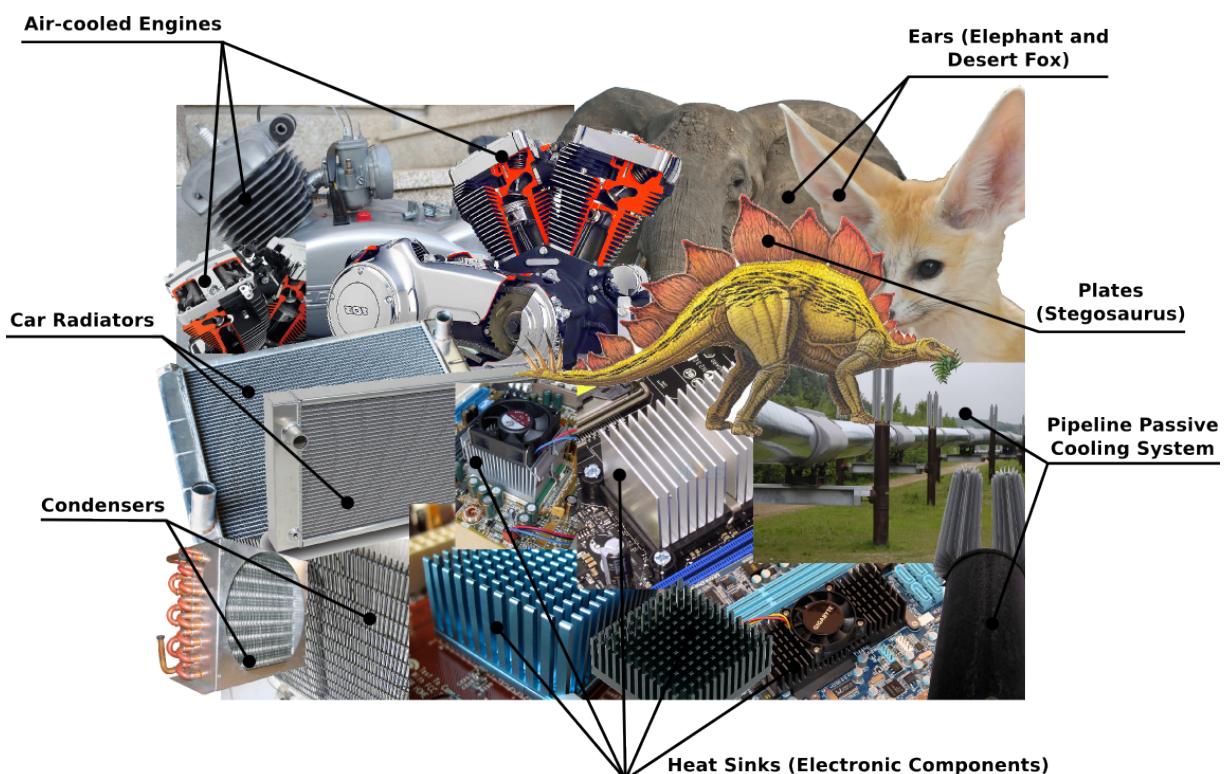
Heat Transfer

Computational Laboratories

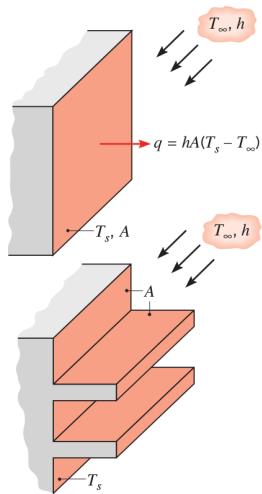
Heat Transfer From Extended Surfaces (Laboratory I)

Exploring the role of geometrical and thermophysical design parameters on the fin performance

Extended Surfaces - Fins: Practical Applications



Extended Surfaces - Fins: Motivation for Application



To increase the rate of heat transfer (q) considering T_s constant:

- Increase h and/or decrease T_∞ ;
- **Increase surface area (A).**

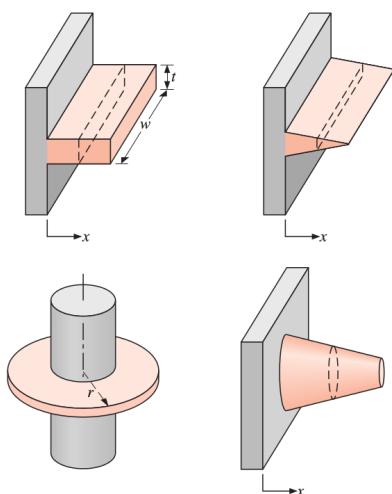
Motivation for Fin Application

Extended surfaces aim to **enhance heat transfer** by an increase in the available surface area for convection (and/or radiation). **Highly recommended when h is small** (gases under free-convection conditions).

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Extended Surfaces - Fins: Configurations

Fin Configuration



Typical Configurations:

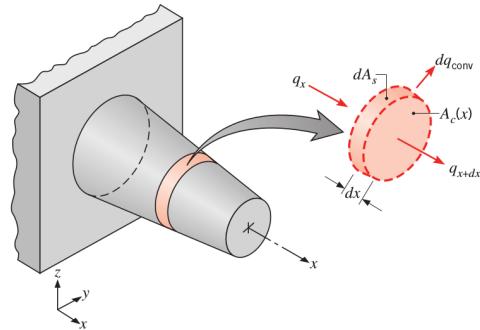
- Straight fins:
 - Uniform Cross Section
 - Non-uniform Cross Section
- Annular fins (non-uniform cross section)
- Pin fins (non-uniform cross-section)

The **selection** of the fin design depends on: space, weight, cost, effect on fluid motion (and consequently on h and pressure drop).

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Fin Equation: Governing Energy Balance Equation

- Equation derived from the application of an energy balance to a differential element.
- Assumptions:
 - one-dimensional conduction;
 - steady-state conditions;
 - constant thermal conductivity;
 - no thermal energy generation;
 - negligible radiative heat losses.



Fin Equation - General Form

$$\frac{d^2 T}{dx^2} + \left(\frac{1}{A_c} \frac{dA_c}{dx} \right) \frac{dT}{dx} - \frac{1}{A_c k} \frac{dA_s}{dx} [T(x) - T_\infty] = 0$$

- The solution of the fin equation provides the temperature distribution along the axial position $T(x)$.

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Fin Equation Applied to Uniform Fins

Fin Equation - General Form

$$\frac{d^2 T}{dx^2} + \left(\frac{1}{A_c} \frac{dA_c}{dx} \right) \frac{dT}{dx} - \frac{1}{A_c k} \frac{dA_s}{dx} [T(x) - T_\infty] = 0$$

Considering:

For fins of uniform cross section:

$$\bullet \frac{dA_c}{dx} = 0$$

- $m^2 = \frac{hP}{kA_c}$ ($P = dA_s/dx$)
- $\xi = x/L$
- $\Theta(\xi) = \frac{\theta(\xi)}{\theta_b} = \frac{T(\xi) - T_\infty}{T(0) - T_\infty}$

Fin Equation for Uniform Fins

$$\frac{d^2 \Theta}{d\xi^2} - (mL)^2 \Theta(\xi) = 0$$

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General Sol. for the Fin Eq. Applied to Uniform Fins

General Solution of the Fin Equation for Uniform Fins

$$\Theta(\xi) = C_1 e^{mL\xi} + C_2 e^{-mL\xi}$$

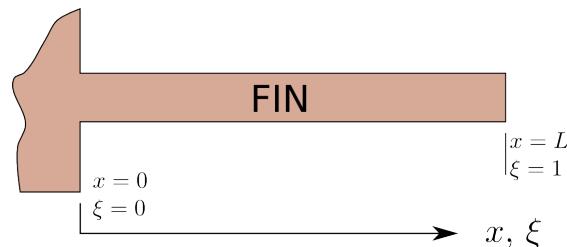
Boundary conditions (BC)

1. Fin base ($\xi = 0$):

- $\Theta(0) = 1$ (Fixed temperature - Dirichlet BC)

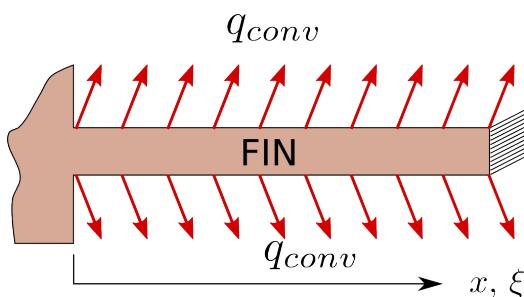
2. Fin tip ($\xi = 1$):

- $\frac{d\Theta}{d\xi} \Big|_{\xi=1} = 0$ (Adiabatic tip - Zero Neumann BC)
- $-k \frac{d\Theta}{d\xi} \Big|_{\xi=1} = h_{tip} L \Theta(1)$ (Active tip - Convection BC)



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Fin Eq. Solution for Uniform Fin with Adiabatic Tip



Normalized Excess Temperature

$$\Theta^a(\xi) = \frac{\cosh [mL(1-\xi)]}{\cosh(mL)}$$

Note that

- $mL = \sqrt{\frac{hP}{kA_c}} L$
- $M = \sqrt{hPkA_c} \theta_b$
 - M corresponds to the heat rate observed for an infinite fin (q_f^i)

Fin Heat Transfer Rate

$$q_f^a = M \tanh(mL)$$

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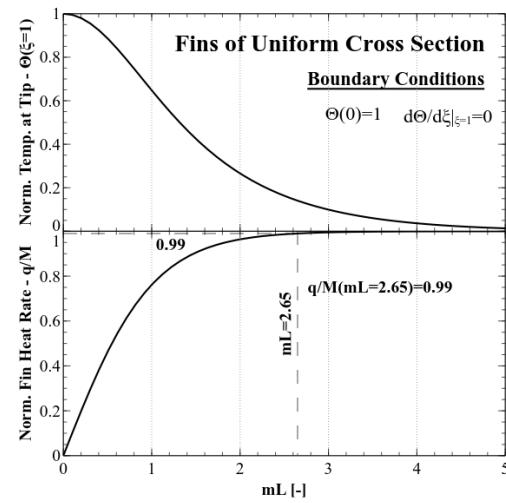
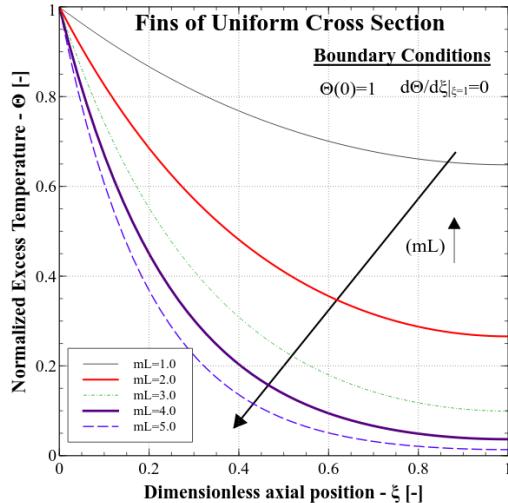
Fin Eq. Solution for Uniform Fin with Adiabatic Tip

Normalized Excess Temperature

$$\Theta^a(\xi) = \frac{\cosh[mL(1-\xi)]}{\cosh(mL)}$$

Normalized Heat Transfer Rate

$$\frac{q_f^a}{M} = \tanh(mL)$$



Heat Transfer From Extended Surfaces (Computational Laboratory I) - 9 of 31

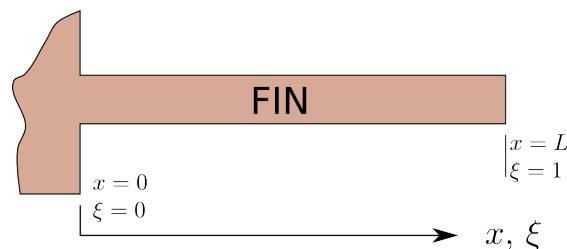
General Sol. for the Fin Eq. Applied to Uniform Fins

General solution of the Fin Equation for Uniform Fins

$$\Theta(\xi) = C_1 e^{mL\xi} + C_2 e^{-mL\xi}$$

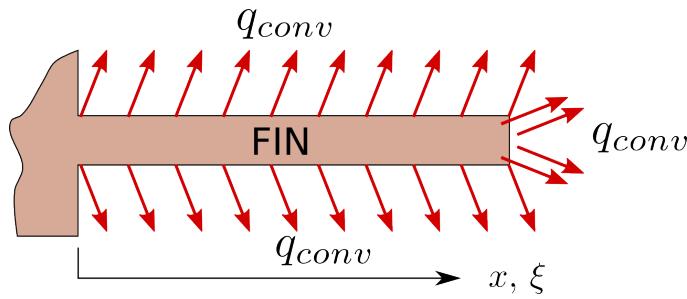
Boundary conditions (BC)

1. **Fin base ($\xi = 0$):**
 - o $\Theta(0) = 1$ (Fixed temperature - Dirichlet BC)
2. **Fin tip ($\xi = 1$):**
 - o $\frac{d\Theta}{d\xi}\Big|_{\xi=1} = 0$ (Adiabatic tip - Zero Neumann BC)
 - o $-k \frac{d\Theta}{d\xi}\Big|_{\xi=1} = h_{tip} L \Theta(1)$ (Active tip - Convection BC)



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Fin Eq. Solution for Uniform Fin with Convective Tip



Normalized Excess Temperature

$$\Theta^c(\xi) = \frac{\cosh[mL(1-\xi)] + (h_{tip}/km)\sinh[mL(1-\xi)]}{\cosh(mL) + (h_{tip}/km)\sinh(mL)}$$

Fin Heat Transfer Rate

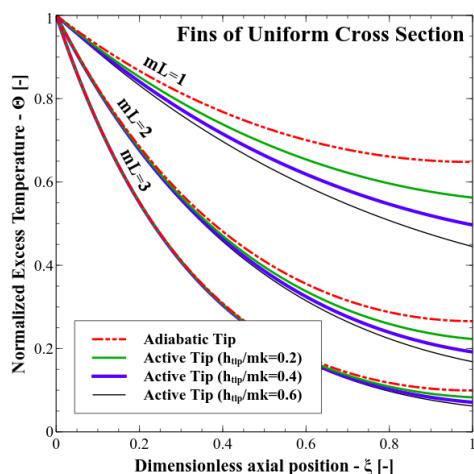
$$q_f^c = M \frac{(h_{tip}/mk) + \tanh(mL)}{1 + (h_{tip}/mk) \tanh(mL)}$$

Note that

- $h_{tip} = 0$: adiabatic tip solution
- Generally $h_{tip} = h$

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Adiabatic vs. Convective Tip Solutions

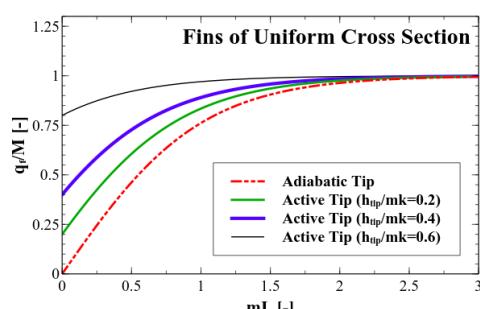


The difference $\Theta^a(\xi) - \Theta^c(\xi)$ increases by:

- increasing h_{tip} for a constant mL ;
- decreasing L for a constant h_{tip} .

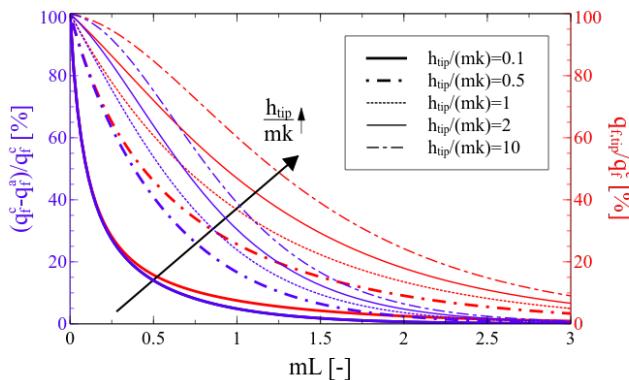
Increasing h_{tip} :

- $q_f^c - q_f^a$ increases;
- $\left. \frac{d\Theta}{d\xi} \right|_{\xi=1}$ increases, i.e. $q_{f,tip}$ increases, since $q_{f,tip} = -k\theta_b \frac{A_c}{L} \left. \frac{d\Theta}{d\xi} \right|_{\xi=1}$.



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Relative importance of the tip convection on the overall heat transfer rate from the fin (1/2)



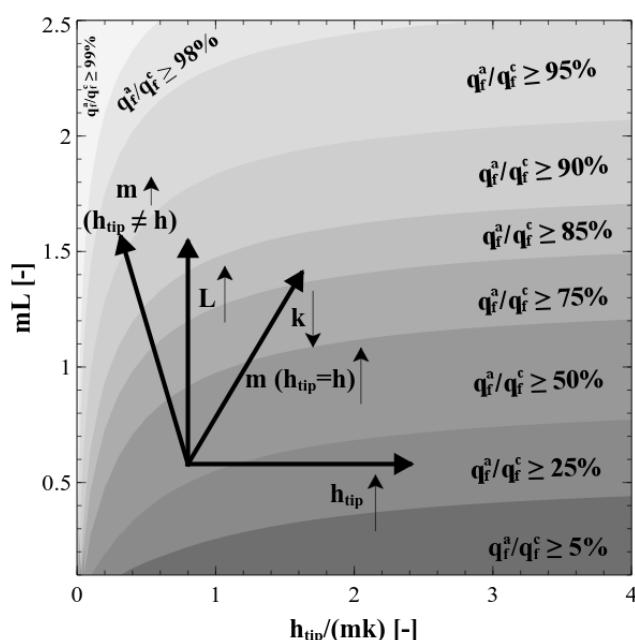
$q_{f,tip}/q_f^c$ decreases:

- increasing the fin length ($L \uparrow$);
- decreasing the convection coefficient at the fin tip ($h_{tip} \downarrow$).

The adiabatic tip solution becomes a suitable approximation for an actual active tip for **low values of $q_{f,tip}/q_f^c$** or **high values of q_f^a/q_f^c** .

- $q_{f,tip} = \frac{q_f^c - q_f^a}{1 - 2\operatorname{sech}(mL)\sinh(\frac{mL}{2})}$
 - $q_{f,tip} \approx q_f^c - q_f^a$ for low mL values.
- $q_{f,tip} = h_{tip}A_c\theta_b\Theta^c(\xi = 1)$
- $\frac{q_{f,tip}}{q_f^c} = \frac{(h_{tip}/km)}{(h_{tip}/km)\cosh(mL) + \sinh(mL)}$

Relative importance of the tip convection on the overall heat transfer rate from the fin (2/2)



The adiabatic tip solution becomes a suitable approximation for an actual active tip for **low values of $q_{f,tip}/q_f^c$** or **high values of q_f^a/q_f^c** .

- $\frac{q_f^a}{q_f^c} = \frac{\tanh(mL)[1 + (h_{tip}/km)\tanh(mL)]}{(h_{tip}/km) + \tanh(mL)}$

q_f^a/q_f^c increases:

- increasing the fin length ($L \uparrow$);
- decreasing h_{tip} ;
- increasing m , that is:
 - increasing h/k ;
 - increasing P/A_c .

Fin Performance Parameters

Fin Effectiveness (ε_f)

$$\varepsilon_f = \frac{q_f}{A_{c,b} h \theta_b}$$

ε_f - ratio between the actual fin heat rate and the heat rate observed without the fin application.

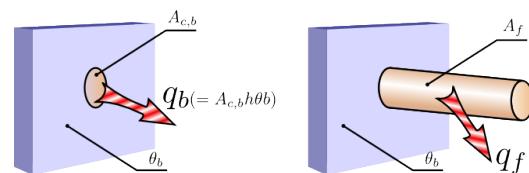
- The application of an extended surface may increase the heat transfer resistance (fin resistance) in relation to the convection resistance of the bare surface ($\varepsilon_f = R_{t,b}/R_{t,f}$).
- In general, $\varepsilon_f < 2$ do not justify the fin application.

Fin Efficiency (η_f)

$$\eta_f = \frac{q_f}{A_f h \theta_b}$$

η_f - ratio between the actual fin heat rate and the maximum (idealized) fin heat rate achieved for $\theta(x) = \theta_b$.

- An efficiency above 90% is attained for most of the fins used in practical applications.

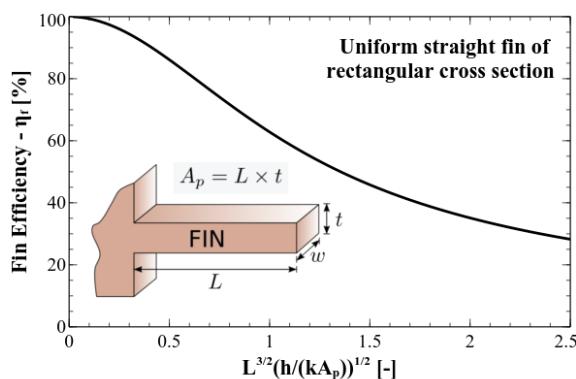


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Performance for the Uniform Fin with Adiabatic Tip

Fin Efficiency (η_f)

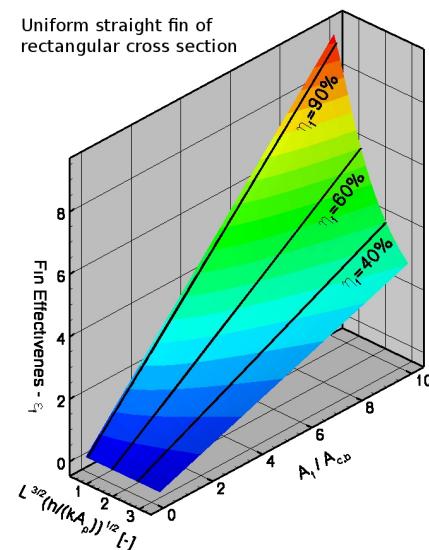
$$\eta_f^a = \frac{\tanh(mL)}{mL} = \int_0^1 \Theta d\xi$$



$$mL \cong L^{3/2} [2h/(kA_p)]^{1/2}, w \gg t$$

Fin Effectiveness (ε_f)

$$\varepsilon_f^a = \frac{A_f}{A_{c,b}} \eta_f^a$$



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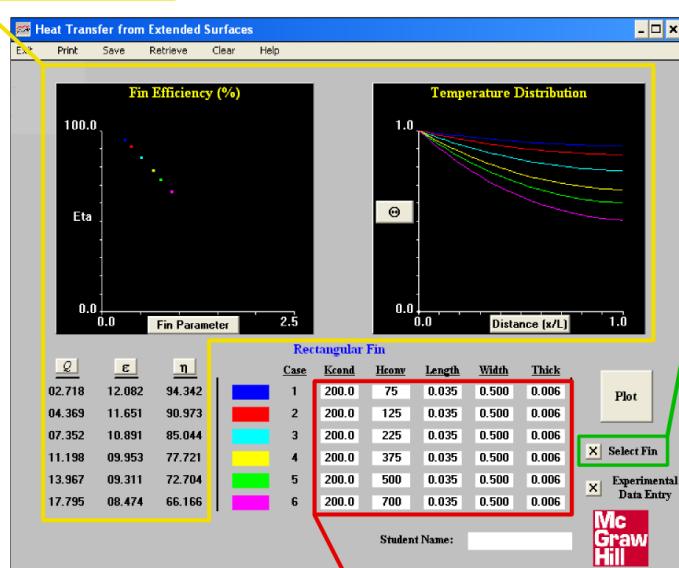
Final Remarks

- The temperature distribution along the fin is evaluated with the fin equation through analytic or numerical means. From the evaluated temperature profile, the fin heat rate, efficiency and effectiveness can be computed.
- The effect of fin design parameters and boundary conditions on the fin temperature distribution, heat rate, and performance parameters registered before for uniform fins is also observed (eventually at a different extent) for fins of non-uniform cross-sectional area.
- For non-uniform fins the integration of the fin equation (governing energy equation) and the evaluation of integration constants result in complex expressions for the temperature distribution. For such reason, only expressions for the fin efficiency are commonly provided in the literature.

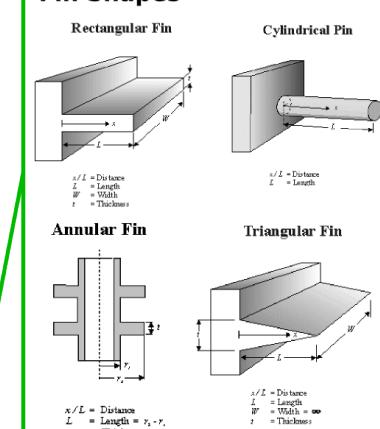
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Exploring the Software

Output - Results



Fin Shapes

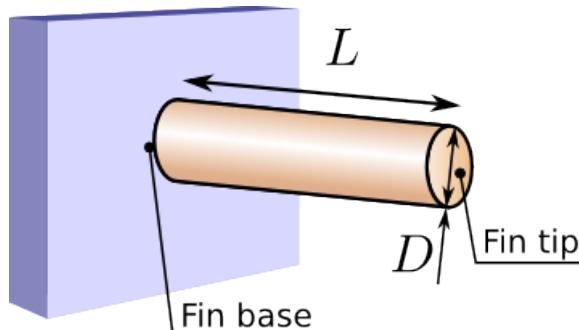


Input (geometrical and thermophysical) Data

- The software solves the fin equation through numerical methods employing the finite volume method.

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Exploring the Software - Uniform Pin Fin



Heat Transfer From Extended Surfaces (Computational Laboratory I) - 19 of 31

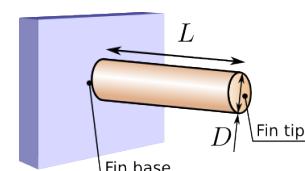
Exploring the Software - Uniform Pin Fin

Role of the thermal conductivity ("Kcond")

Consider a pin fin of uniform cross section ("Cylindrical Pin") with an adiabatic tip

1. Reference Data

Themo. Properties	Geom. Properties
$k = 20 \text{ W}/(\text{mK})$	$L = 0.035 \text{ m}$
$h = 100 \text{ W}/(\text{m}^2\text{K})$	$D = 0.015 \text{ m}$



2. Thermal conductivity values

- $k_1 = 20 \text{ W}/(\text{mK})$
- $k_2 = 30 \text{ W}/(\text{mK})$
- $k_3 = 50 \text{ W}/(\text{mK})$
- $k_4 = 100 \text{ W}/(\text{mK})$
- $k_5 = 200 \text{ W}/(\text{mK})$

3. Effect on:

- Normalized Excess Temperature ($\Theta(\xi)$);
- Fin Heat Rate ($Q = q_f/\theta_b$);
- Fin Efficiency (η_f);
- Fin Effectiveness (ε_f).

Heat Transfer From Extended Surfaces (Computational Laboratory I) - 20 of 31

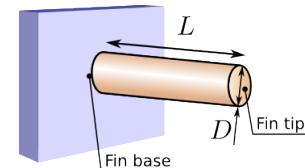
Exploring the Software - Uniform Pin Fin

Role of the convection heat transfer coefficient ("Hconv")

Consider a pin fin of uniform cross section ("Cylindrical Pin") with an adiabatic tip

1. Reference Data

Themo. Properties	Geom. Properties
$k = 20 \text{ W}/(\text{mK})$	$L = 0.035 \text{ m}$
$h = 100 \text{ W}/(\text{m}^2\text{K})$	$D = 0.015 \text{ m}$



2. Convection coefficient values

- $h_1 = 100 \text{ W}/(\text{m}^2\text{K})$
- $h_2 = 150 \text{ W}/(\text{m}^2\text{K})$
- $h_3 = 200 \text{ W}/(\text{m}^2\text{K})$
- $h_4 = 300 \text{ W}/(\text{m}^2\text{K})$
- $h_5 = 400 \text{ W}/(\text{m}^2\text{K})$

3. Effect on:

- Normalized Excess Temperature ($\Theta(\xi)$);
- Fin Heat Rate ($Q = q_f/\theta_b$);
- Fin Efficiency (η_f);
- Fin Effectiveness (ε_f).

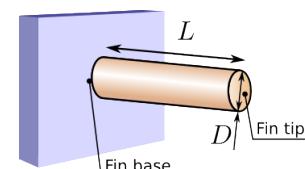
Exploring the Software - Uniform Pin Fin

Role of the fin length ("Length")

Consider a pin fin of uniform cross section ("Cylindrical Pin") with an adiabatic tip

1. Reference Data

Themo. Properties	Geom. Properties
$k = 20 \text{ W}/(\text{mK})$	$L = 0.035 \text{ m}$
$h = 100 \text{ W}/(\text{m}^2\text{K})$	$D = 0.015 \text{ m}$



2. Fin length values

- $L_1 = 0.035 \text{ m}$
- $L_2 = 0.04 \text{ m}$
- $L_3 = 0.05 \text{ m}$
- $L_4 = 0.06 \text{ m}$
- $L_5 = 0.07 \text{ m}$

3. Effect on:

- Normalized Excess Temperature ($\Theta(\xi)$);
- Fin Heat Rate ($Q = q_f/\theta_b$);
- Fin Efficiency (η_f);
- Fin Effectiveness (ε_f).

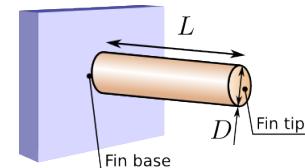
Exploring the Software - Uniform Pin Fin

Role of the fin diameter ("Diam")

Consider a pin fin of uniform cross section ("Cylindrical Pin") with an adiabatic tip

1. Reference Data

Themo. Properties	Geom. Properties
$k = 20 \text{ W}/(\text{mK})$	$L = 0.035 \text{ m}$
$h = 100 \text{ W}/(\text{m}^2\text{K})$	$D = 0.015 \text{ m}$



2. Fin diameter values

- $D_1 = 0.015 \text{ m}$
- $D_2 = 0.02 \text{ m}$
- $D_3 = 0.03 \text{ m}$
- $D_4 = 0.04 \text{ m}$
- $D_5 = 0.05 \text{ m}$

3. Effect on:

- Normalized Excess Temperature ($\Theta(\xi)$);
- Fin Heat Rate ($Q = q_f/\theta_b$);
- Fin Efficiency (η_f);
- Fin Effectiveness (ε_f).

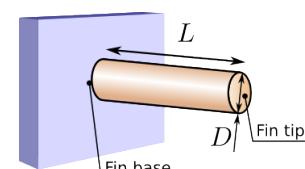
Exploring the Software - Uniform Pin Fin

Effect of the tip boundary condition

Consider a pin fin of uniform cross section ("Cylindrical Pin")

1. Reference Data

Themo. Properties	Geom. Properties
$k = 20 \text{ W}/(\text{mK})$	$L = 0.035 \text{ m}$
$h = 100 \text{ W}/(\text{m}^2\text{K})$	$D = 0.015 \text{ m}$



2. Prescribed boundary condition

- Adiabatic tip
- Convective tip

3. Effect on:

- Normalized Excess Temperature ($\Theta(\xi)$);
- Fin Heat Rate ($Q = q_f/\theta_b$);
- Fin Efficiency (η_f);
- Fin Effectiveness (ε_f).

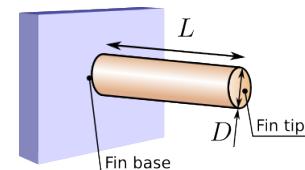
Exploring the Software - Uniform Pin Fin

Role of the fin diameter ("Diam") on q_f^a/q_f^c

Consider a pin fin of uniform cross section ("Cylindrical Pin")

1. Reference Data

Themo. Properties	Geom. Properties
$k = 20 \text{ W}/(\text{mK})$	$L = 0.035 \text{ m}$
$h = 100 \text{ W}/(\text{m}^2\text{K})$	$D = 0.015 \text{ m}$



2. Diameter values

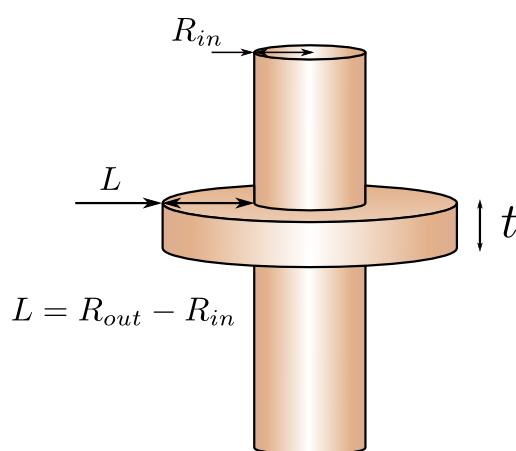
- $D_1 = 0.015 \text{ m}$
- $D_2 = 0.02 \text{ m}$
- $D_3 = 0.03 \text{ m}$
- $D_4 = 0.04 \text{ m}$
- $D_5 = 0.05 \text{ m}$

3. Effect on q_f^a/q_f^c

D	$Q^a = q_f^a/\theta_b$	$Q^c = q_f^c/\theta_b$	q_f^a/q_f^c
D_1	0.110	0.115	≈ 0.959
D_2	0.160	0.169	≈ 0.947
D_3	0.262	0.292	≈ 0.897
D_4	0.368	0.430	≈ 0.856
D_5	0.475	0.583	≈ 0.815

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Exploring the Software - Annular Fin



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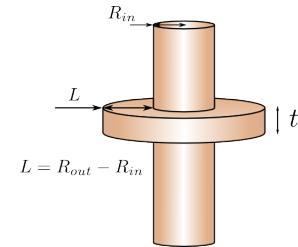
Exploring the Software - Annular Fin

Role of the thermal conductivity ("Kcond")

Consider an annular fin with an adiabatic tip

1. Reference Data

Themo. Properties	Geom. Properties
$k = 20 \text{ W}/(\text{mK})$	$R_{in} = 0.035 \text{ m}$
$h = 100 \text{ W}/(\text{m}^2\text{K})$	$R_{out} = 0.050 \text{ m}$
	$t = 0.001 \text{ m}$



2. Thermal conductivity values

- $k_1 = 20 \text{ W}/(\text{mK})$
- $k_2 = 30 \text{ W}/(\text{mK})$
- $k_3 = 50 \text{ W}/(\text{mK})$
- $k_4 = 100 \text{ W}/(\text{mK})$
- $k_5 = 200 \text{ W}/(\text{mK})$

3. Effect on:

- Normalized Excess Temperature ($\Theta(\xi)$);
- Fin Heat Rate ($Q = q_f/\theta_b$);
- Fin Efficiency (η_f);
- Fin Effectiveness (ε_f).

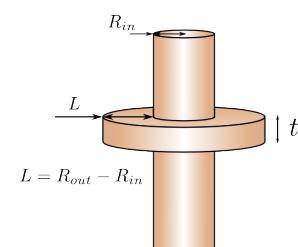
Exploring the Software - Annular Fin

Role of the convection heat transfer coefficient ("Hconv")

Consider an annular fin with an adiabatic tip

1. Reference Data

Themo. Properties	Geom. Properties
$k = 20 \text{ W}/(\text{mK})$	$R_{in} = 0.035 \text{ m}$
$h = 100 \text{ W}/(\text{m}^2\text{K})$	$R_{out} = 0.050 \text{ m}$
	$t = 0.001 \text{ m}$



2. Convection coefficient values

- $h_1 = 100 \text{ W}/(\text{m}^2\text{K})$
- $h_2 = 150 \text{ W}/(\text{m}^2\text{K})$
- $h_3 = 200 \text{ W}/(\text{m}^2\text{K})$
- $h_4 = 300 \text{ W}/(\text{m}^2\text{K})$
- $h_5 = 400 \text{ W}/(\text{m}^2\text{K})$

3. Effect on:

- Normalized Excess Temperature ($\Theta(\xi)$);
- Fin Heat Rate ($Q = q_f/\theta_b$);
- Fin Efficiency (η_f);
- Fin Effectiveness (ε_f).

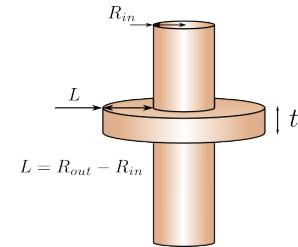
Exploring the Software - Annular Fin

Role of the fin outside radius ("Rout")

Consider an annular fin with an adiabatic tip

1. Reference Data

Themo. Properties	Geom. Properties
$k = 20 \text{ W}/(\text{mK})$	$R_{in} = 0.035 \text{ m}$
$h = 100 \text{ W}/(\text{m}^2\text{K})$	$R_{out} = 0.050 \text{ m}$
	$t = 0.001 \text{ m}$



2. Outside radius values

- $R_{out,1} = 0.050 \text{ m}$
- $R_{out,2} = 0.055 \text{ m}$
- $R_{out,3} = 0.060 \text{ m}$
- $R_{out,4} = 0.070 \text{ m}$
- $R_{out,5} = 0.080 \text{ m}$

3. Effect on:

- Normalized Excess Temperature ($\Theta(\xi)$);
- Fin Heat Rate ($Q = q_f/\theta_b$);
- Fin Efficiency (η_f);
- Fin Effectiveness (ε_f).

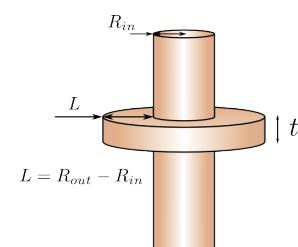
Exploring the Software - Annular Fin

Role of the fin thickness ("Thick")

Consider an annular fin with an adiabatic tip

1. Reference Data

Themo. Properties	Geom. Properties
$k = 20 \text{ W}/(\text{mK})$	$R_{in} = 0.035 \text{ m}$
$h = 100 \text{ W}/(\text{m}^2\text{K})$	$R_{out} = 0.050 \text{ m}$
	$t = 0.001 \text{ m}$



2. Outside radius values

- $t_1 = 0.0010 \text{ m}$
- $t_2 = 0.0015 \text{ m}$
- $t_3 = 0.0020 \text{ m}$
- $t_4 = 0.0030 \text{ m}$
- $t_5 = 0.0040 \text{ m}$

3. Effect on:

- Normalized Excess Temperature ($\Theta(\xi)$);
- Fin Heat Rate ($Q = q_f/\theta_b$);
- Fin Efficiency (η_f);
- Fin Effectiveness (ε_f).

Useful Relations

1. Fin Temperature Distribution - Θ, θ, T

$$\Theta(\xi) = \frac{\theta(\xi)}{\theta_b} = \frac{T(\xi) - T_\infty}{T(\xi = 0) - T_\infty}$$

$\Theta(\xi)$ - Normalized excess temperature

θ_b - Excess temperature at the fin base

2. Fin Heat Rate - q_f

$$q_f = \theta_b h \underbrace{\int_{A_f} \Theta(\xi) dA_s}_{Q = \frac{q_f}{\theta_b}}$$

q_f^a - fin heat rate considering an adiabatic tip

q_f^c - fin heat rate considering a convective tip

A_f - convective fin area

3. Fin Efficiency - η_f

$$\eta_f = \frac{q_f}{A_f h \theta_b} = \frac{Q}{A_f h}$$

4. Fin Effectiveness - ε_f

$$\varepsilon_f = \frac{q_f}{A_{c,b} h \theta_b} = \eta_f \frac{A_f}{A_{c,b}}$$